

✓ On page 4, line 16, please replace "dissolving" with --dissolving--.

✓ On page 5, line 31, please replace "pharma-ceutical" with --pharmaceutical--.

✓ On page 6, line 1, please replace "raw" with --crude--.

✓ On page 6, line 4, please replace "raw" with --crude--.

✓ On page 6, line 10, please replace "raw" with --crude--.

✓ On page 7, line 4, please replace "the man" with --one--.

In the Claims:

Please add the following new claims 24-47 and cancel claims 1-23 without prejudice:

24. (new) A process for the isolation and purification of HMG-CoA reductase inhibitors from mycelium biomass which comprises:
- clarifying a mycelium broth and concentrating the clarified broth to a lower volume, *known*
 - acidifying of the concentrate to a pH value in the range of 4.5 to 7.5, followed by extracting the HMG-CoA reductase inhibitor with ethyl acetate, *known*
 - optionally performing lactonization, *known*
 - crystallization of the HMG-CoA reductase inhibitor from a water-miscible or water-soluble organic solvent, and
 - crystallization of the HMG-CoA reductase inhibitor from an organic solvent having (limited) miscibility or solubility with water.

25. (new) The process according to claim 24, further comprising, before clarifying the mycelium biomass broth:

- dissolving the HMG-CoA reductase inhibitor from a mycelium biomass at pH value between 9.5 and 13 into fermentation liquor, and
- adjusting the broth to a pH value between 7.5 and 8.5.

26. (new) The process according to claim 25, wherein the dissolving step is carried out at a

temperature in the range of 10 to 40°C for less than one hour.

27. (new) The process according to claim 24, wherein clarifying the mycelium broth is carried out by removing the mycelium from the broth by means of filtration.

28. (new) The process according to claim 24, wherein said clarified broth is concentrated by means of reverse osmosis.

29. (new) The process according to claim 24, wherein the concentrate is acidified to a pH value in the range of 5.5 to 7.5.

30. (new) The process according to claim 24, wherein the concentrate is acidified to a pH value in the range of 6.0 to 7.0.

31. (new) The process according to claim 24, wherein the HMG-CoA reductase inhibitor which is extracted from ethyl acetate and optionally lactonized is subjected to a purification step by adsorption chromatography.

32. (new) The process according to claim 31, wherein a mixture of acetonitrile and water is used as the mobile phase for adsorption chromatography.

33. (new) The process according to claim 24, wherein the order of the crystallization steps is reversed.

34. (new) The process according to claim 24, wherein the water-miscible or water-soluble organic solvent used in the crystallization step is acetone or a low alkyl alcohol.

35. (new) The process according to claim 24, wherein the crystallization step from a water-miscible or water-soluble organic solvent comprises dissolving the HMG-CoA reductase

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inhibitor in acetone, and then adding water thereto.

36. (new) The process according to claim 24, wherein the crystallization step from an organic solvent having limited miscibility or solubility with water comprises dissolving the HMG-CoA reductase inhibitor in said organic solvent at a concentration of 10 to 35 g/l, and removing one-third to three-fourth of said organic solvent.

37. (new) The process according to claim 24, wherein the organic solvent having limited miscibility or solubility with water used in the crystallization step is ethyl acetate.

38. (new) The process according to claim 24, wherein HMG-CoA reductase inhibitors are obtained having a purity higher than 99.6%.

39. (new) The process according to claim 24, wherein the HMG-CoA reductase inhibitor is selected to be lovastatin.

40. (new) A process for the purification of HMG-CoA reductase inhibitors which comprises subjecting the HMG-CoA reductase inhibitor to combined crystallization steps, which comprises crystallization from an water-miscible or water-soluble ^{solvent} and crystallization from an organic solvent having limited miscibility or solubility with water (as final polishing steps) to obtain HMG-CoA reductase inhibitors having a purity higher than 99.6%.

41. (new) The process according to claim 40, wherein the obtained HMG-CoA reductase inhibitors have purity higher than 99.7 %.

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42. (new) The process according to claim 40, wherein acetone or a low alkyl alcohol is used as the water-miscible or water-soluble organic solvent.

43. (new) The process according to claim 40, wherein the crystallization from a water-miscible